



### Hydrogen Sulfide Removal From Biogas & Landfill Gas

Basics of H2s & Commercial Removal Technologies





# Agenda

#### Hydrogen Sulfide Removal From Biogas and Landfill Gas

Basics of H<sub>2</sub>S and Commercial Removal Technologies

**Presented By** 



### **01** Basics of Hydrogen Sulfide

- What is it, where does it originate?
- What is the impact of H2S, What are the regulations?

# **02** Commercial Options for H2S Removal

- Integral with CO2 Removal (Molecular Gate<sup>™</sup>, Water Wash)
- Regenerative Media Systems
- Replaceable Media Systems

**03** Deep Dive: Controlling the Process Parameters to Enhance Replaceable Media system

#### **Basics of Hydrogen Sulfide**

- What is it, where does it originate?
- What is the impact of  $H_2S$
- What are the regulations?



#### What Is Hydrogen Sulfide?

- Colorless Gas that is an Irritant and Dangerous Asphyxiant
  - Characteristically a "rotten egg" smell
  - Can be detected in concentrations as low as 0.1-1.5 ppm
- Irritant and asphyxiant
  - NIOSH PEL (Permissible Exposure Level): 10 ppm
  - NIOSH IDLH (Immediately Dangerous to Life and Health): 100 ppm
- Flammable in a wide range of concentrations
  - Explosion Level in air 4% 44% v/v
  - Heavier than air tends to collect in low-lying area



#### **Sources of Hydrogen Sulfide**

- Municipal Solid Waste Landfills
  - Waste Water Treatment Plant sludge
  - Pulp & paper mill wastes
  - Gypsum/drywall
    - Alone and as part of Construction and Demolition waste streams
    - Construction and Demolition fines (small particles)
    - Major Storm event (hurricanes, tornado) debris can change landfill characteristics quickly
- Agricultural Digesters
  - Feed for Livestock influences H<sub>2</sub>S Content in Manure
  - Rendering waste



#### H2S impact on Downstream Equipment

- Detrimental to metallic components
- Causes Deposits on Valves
- H<sub>2</sub>S combustion in Flare or Thermal Oxidizer leads to SO<sub>2</sub> formation
  - Air Permits of the Biogas Site affected by SO<sub>2</sub> Emissions
  - 100 TPY (tons per year) of SO<sub>2</sub> results in Major Source Status for Air Permitting by local EPA



#### H<sub>2</sub>S Process Selection Design Considerations

- Total Biogas flow
  - Current flow, anticipated peak flow, and minimum flow
  - Project flow 20 years outward
- $H_2S$  concentration projection at the noted flows
- Requirements for treated gas and waste gas
  - Flaring of waste gas Air Permit
  - RNG Pipeline standard, CNG Vehicle Fuel requirement
- Feed gas pressure and anticipated system pressure drop
  - Design feed blower to deliver at needed pressure
  - How much drop should I expect to see across the treatment system?
- Feed gas temperature requirement
- Available equipment footprint at site
- Scalability grow with anticipated biogas flow?.



**Equipment Options for Commercial H<sub>2</sub>S Removal** 

- Integral with  $CO_2$  Removal (Molecular Gate<sup>TM</sup>, Water Wash)
- Regenerative Media Systems
- Replaceable Media Systems



Molecular Gate<sup>™</sup> Pressure Swing Adsorption by Guild Associates

- H<sub>2</sub>S removed with CO<sub>2</sub>, siloxanes, VOCs and water
- Media is regenerated using vacuum compression
- Media lasts the life of equipment (20+ years)
- H<sub>2</sub>S is combusted in the TOX/Flare with other contaminants
- Field proven for feed gas of 7000 PPM reduced to pipeline standards
- Requires air permits for H<sub>2</sub>S combustion



Water Wash CO<sub>2</sub> Removal Technology

- H<sub>2</sub>S removed with CO<sub>2</sub> in water wash tower
- CO<sub>2</sub> is released to atmosphere/burned in TOX
- Media lasts the life of equipment (20+ years)
- H<sub>2</sub>S accumulates in water, needs to be treated and replaced

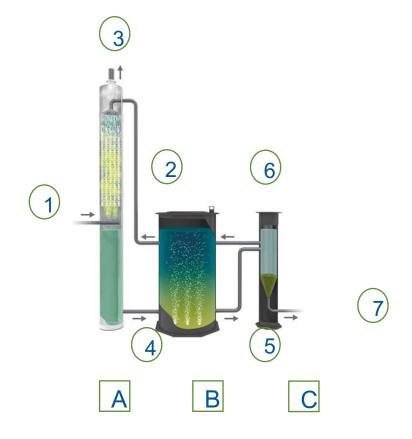


#### **Regenerative Media Systems**

- Wet scrubber application for feed biogas
- Liquid is regenerated by various methods
- "Caustic" solution chelated iron, hydroxide, bicarbonate ...
- Solution can be recovered and recycled
- Chemical process requires monitoring
- Biological regeneration is an option



#### **Example of Regenerative Process**



- A. Absorber/contactor
- B. Reactor
- C. Settling
- 1. Raw (sour) LFG
- 2. Wash solution
- 3. Treated (sweet) LFG
- 4. High-sulfur liquid
- 5. Concentrated-sulfur liquid
- 6. Recovered wash solution
- 7. Elemental sulfur paste



#### **Replaceable Media Systems – Activated Carbon Media**

Feed gas passes through a vessel of Activated Carbon

- Media adsorbs H<sub>2</sub>S in pores of media
- Media tends to adsorb other non-target chemicals, reducing H<sub>2</sub>S capacity
- Spent media can typically be disposed in landfills, can possibly be classified as Hazardous
- Elemental sulfur is "fixed" and doesn't leach back into waste
- Media generally removes about 25% of its weight in  $H_2S$



#### **Replaceable Media Systems – Catalytic Reaction Media**

Feed gas passes through a vessel of Catalytic Reactive Media

- Feed gas fed through media
- Sequential chemical reaction enabled by media
  - First with water, then oxygen
  - Results in elemental sulfur deposited on media
- Iron Sponge media prone to agglomerating particles into large bricks, resulting in less capacity, higher removal costs, higher pressure drops
- BSR-050 from Guild Associates not susceptible to bricking
- Media capacity typically 10-15% for Iron Sponge, 120% for BSR-050
- Spent media can typically be disposed in landfills



### **Problem Statement and Objectives**

Problem:

• H<sub>2</sub>S Removal is problematic, expensive and unpredictable

#### **Objectives**:

- Maximize utilization of H<sub>2</sub>S scavenger media to reduce cost and logistics burdens associated with natural gas purification
- Relationships between [O<sub>2</sub>], [H<sub>2</sub>O], [H<sub>2</sub>S] and temperature on media performance





#### **Basics of Media Reaction Chemistry**

H<sub>2</sub>S Reaction Chemistry

$$M-O + H_2S \rightarrow M-S + H_2O$$

 $M-S + \frac{1}{2} O_2 \rightarrow M-O + S$ 

Two Reactions:

- Metal sulfide formation very fast
- Site regeneration slower and must be balanced

Reaction is Catalytic

- O<sub>2</sub> necessary for reaction
- Reaction slows then terminates as elemental sulfur blocks reaction sites

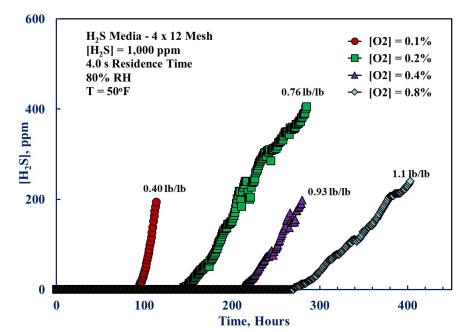


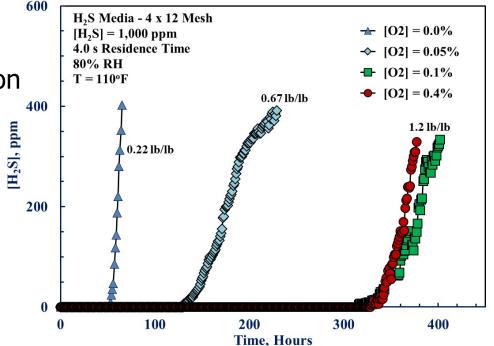
BSR-050 H2S Media



#### **Effects of [O<sub>2</sub>] and Temperature**

- More O<sub>2</sub> required at lower T to maximize capacity
- Operation at increased T allows for operation at lower O<sub>2</sub>



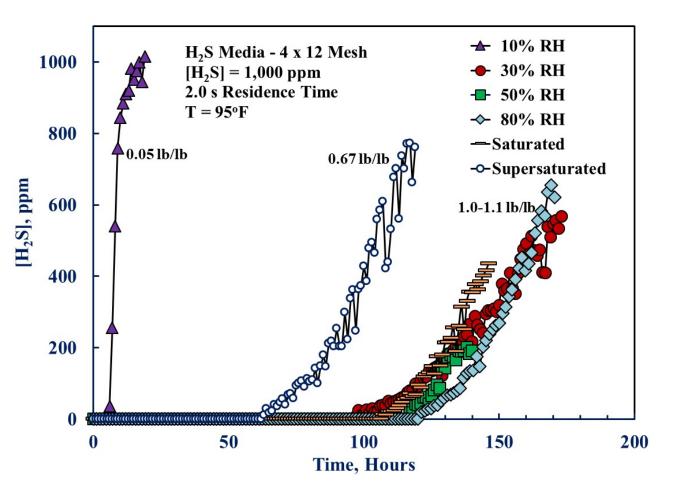




### Effects of [H<sub>2</sub>O]

H<sub>2</sub>O is necessary for the reaction to proceed – active site is a hydrated metal oxide/hydroxide

- Fill pores of media with water, preventing H<sub>2</sub>S from accessing active sites within media – leading to decreased capacity
- Force reaction to external surface, leading to "bricking" and clumping of media
- Drying media does not return capacity media is "eggshelled" with sulfur and/or iron sulfide





#### Effects of [H<sub>2</sub>O] – Case Study





Spent media removed from vessel where water had significantly condensed  $H_2S$  removal capacity = 0.78 lb/lb

Spent media in vessel from process where water condensation was minimized H<sub>2</sub>S removal capacity = 1.15 lb/lb



#### Summary of Temperature, O<sub>2</sub> and H<sub>2</sub>O

Temperature,  $[H_2O]$ ,  $[O_2]$  and  $[H_2S]$  in the process stream will impact  $H_2S$  removal capability of media

- Higher temperatures required for optimal operation when [O<sub>2</sub>] is low
- Prolonged periods of water condensation in bed detrimental to performance
  - Reduced H<sub>2</sub>S removal capacity
  - "Bricking"



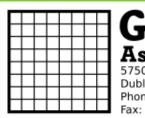


### **Thank You!**

Please Contact Guild Associates should you have questions!

### Guild Associates, Inc.

www.GuildAssociates.com H2S@GuildAssociates.com 614-798-8215



**Gatild** Associates, Inc. 5750 Shier Rings Road Dublin, OH 43016 Phone: (614) 798-8215 Fax: (614) 798-1972